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Thiosemicarbazone modified zeolitic imidazolate framework (TSC-ZIF) for mercury(II) removal from water†

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Zeolitic imidazolate frameworks (ZIF-8), and their derivatives, have been drawing increasing attention due to their thermal and chemical stability. The remarkable stability of ZIF-8 in aqueous and high pH environments renders it an ideal candidate for the removal of heavy metals from wastewater. In this study, we present the preparation of novel aldehyde-based zeolitic imidazolate frameworks (Ald-ZIF) through the integration of mixed-linkers: 2-methylimidazole (MIM) and imidazole-4-carbaldehyde (AldIM). The prepared Ald-ZIFs were post-synthetically modified with bithiosemicarbazide (Bisthio) and thiosemicarbazide (Thio) groups, incorporating thiosemicarbazone (TSC) functionalities to the core of the framework. This modification results in the formation of TSC-functionalized ZIF derivatives (TSC-ZIFs). Thiosemicarbazones are versatile metal chelators, hence, adsorption properties of TSC-ZIFs for the removal of mercury(II) from water were explored. Removal of mercury(II) from homoionic aqueous solutions, binary and tertiary systems in competition with lead(II) and cadmium(II) under ambient conditions and neutral pH are reported in this study. $\text{MIM}_{3.5}\text{:Thio}_1\text{:Zn}$ improved the removal efficiency of mercury(II) from water, up to 97% in two hours, with an adsorption capacity of 1667 mg g^{-1} . Desorption of mercury(II) from $\text{MIM}_{3.5}\text{:Thio}_1\text{:Zn}$ was achieved under acidic conditions, regenerating $\text{MIM}_{3.5}\text{:Thio}_1\text{:Zn}$ for five cycles of mercury(II) removal. TSC-ZIF derivatives, designed and developed here, represent a new class of dynamically functionalized adsorption material displaying the advantages of simplicity, efficiency, and reusability.

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Introduction

Metal-organic frameworks (MOFs) are a class of adsorbent materials composed of metal cations, connected to polytopic organic linkers *via* coordination bonds. MOFs,¹⁻³ as porous crystalline materials, combine high porosity, large surface area, flexible pore size and shape,^{4,5} and in most cases, a high stability,⁶ with simple, economical and convenient direct synthetic routes.⁷⁻⁹ The porous structure exhibited by MOFs offers large surface areas, reaching $\sim 5200 \text{ m}^2 \text{ g}^{-1}$,¹⁰ and variety of pore dimensions and topologies.¹¹ All the before mentioned properties render MOFs suitable candidates for catalysis,¹²⁻¹⁶ separation,^{17,18} gas storage,¹⁹⁻²¹ and drug delivery^{19,22-28} among other applications.^{16,29-32}

The flexibility of the coordination bond, joining the organic linker to metal ion, permits chemical modulations through post-synthetic modification (PSM) of the metal-organic framework. This promotes MOFs to high performance, tailor-made materials.³³ PSM, ranging from carrying out chemical transformation³⁴⁻³⁶ or exchange on pre-synthesized materials,^{37,38} has emerged as a powerful method for functionalizing MOFs.^{39,40}

Zeolitic imidazolate frameworks (mainly, ZIF-8) received much attention due to their thermal and chemical stability which makes them ideal candidates for further adjustment of their physical and chemical features to attain satisfactory performances in a wide range of potential applications.⁴¹⁻⁴³ ZIF-8 structures have been prepared using different approaches, mainly hydro and solvothermal.⁴⁴⁻⁴⁶ The remarkable stability of ZIF-8 in aqueous and high pH environments renders it an ideal candidate for the removal of heavy metals from wastewater.⁴⁷

Heavy metals, in general, are toxic to all living organisms.⁴⁸ Mercury, in particular, is considered to be extremely dangerous due to high solubility and bioaccumulation properties.^{49,50} Different techniques have been developed for the removal of heavy metals from contaminated wastewater,^{51,52} such as chemical precipitation,⁵³ membrane filtration,⁵⁴ electrochemical treatments,^{55,56} adsorption^{57,58} and ion exchange.^{59,60} Removal of mercury cations from contaminated wastewater has

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been recently achieved using novel sulfur-functionalized MOFs,^{61–63} adsorption parameters of these MOFs are presented in Table 1. Relevant parameters include maximum mercury adsorption capacity (mg g^{-1}), retention time (minutes), and pH of the medium characterising HKUST-1,⁶² thiol-functionalized ZIF-90 (ZIF-90-SH),⁶⁴ UiO-66-NHC(S)NHMe,⁶⁵ FJI-H12⁶⁶ and other robust MOFs⁶⁷ are presented in the table. The most recent example of an efficient Hg(II) adsorption material is using hybrid material – ZnS with ZIF-8 on filter paper. The high sulfur content in the hybrid material exhibits outstanding adsorption of Hg(II), where the removal was achieved through simple filtration of contaminated water using the monolith ZnS-ZIF-8.⁶⁸

This study presents the preparation of a new class of aldehyde modified ZIF-8 derivatives (Ald-ZIF), which were further functionalized with thiosemicarbazone (TSC) groups for the removal of mercury(II) ions from water. These Ald-ZIF were prepared through the integration of mixed-linkers: 2-methylimidazole (MIM) and imidazole-4-carbaldehyde (AldIM). The linkers were combined in two ratios ($x_1 = 15, y_1 = 1$ and $x_2 = 3.5, y_2 = 1$, where x and y represent the relative contents of MIM and AldIM, respectively) to yield two Ald-ZIF: $\text{MIM}_{15}:\text{AldIM}_1:\text{Zn}$ and $\text{MIM}_{3.5}:\text{AldIM}_1:\text{Zn}$. The major component in all prepared Ald-ZIF is MIM, to retain the chemical and physical properties originally exhibited by ZIF-8. Incorporation of AldIM allows for further functionalization of the ZIF's framework, through post-synthetic modification (PSM). Accordingly, the prepared $\text{MIM}_x:\text{AldIM}_y:\text{Zn}$ were post-synthetically modified with two thiosemicarbazide based functionalities; bis ($\text{NH}_2\text{-NH-CS-NH-NH}_2$) and thio ($\text{NH}_2\text{-NH-CS-NH}_2$) semicarbazones, through the condensation of the aldehyde (in AldIM) to bis/thiosemicarbazide. This successful PSM resulted in the formation of four new thiosemicarbazone zeolitic imidazole framework derivatives (TSC-ZIF), as demonstrated in Scheme 1.

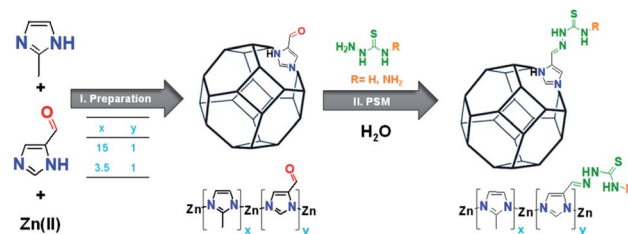
Results and discussion

Aldehyde modified ZIF-8 (Ald-ZIF) derivatives were successfully prepared through modifying the synthetic procedure of ZIF-8.⁶⁹ Simultaneous incorporation of commercially available 2-methylimidazole (MIM) and imidazole-4-carbaldehyde (AldIM) in two different ratios ($x_1 = 15, y_1 = 1$ and $x_2 = 3.5, y_2 = 1$) yielded

Table 1 Comparison of maximum mercury(II) adsorption capacity q_{max} (mg g^{-1}), pH, and adsorption time (min) of TSC-ZIF ($\text{MIM}_{3.5}:\text{Thio}_1:\text{Zn}$) with previously reported sulfur-functionalized MOFs^a

MOF	q_{max} (mg g^{-1})	pH	t (min)	Ref.
Thiol-HKUST-1	714	—	120	62
ZIF-90-SH	22	—	1440	64
UiO-66-NHC(S)R*	769	—	240	65
FJI-H12	440	7	60	66
Zr-MSA	734	5	5	67
ZnS-ZIF-8	925.9	5	<2	68
$\text{MIM}_{3.5}:\text{Thio}_1:\text{Zn}$	1667	7	30	This study

^a R* = NHCH_3 .



Scheme 1 Schematic illustration of (I) preparation of the two Ald-ZIFs ($\text{MIM}_x:\text{AldIM}_y:\text{Zn}$) and (II) post-synthetic modification (PSM) of Ald-ZIFs to obtain TSC-ZIFs through the incorporation of thiosemicarbazone derivatives (bisthiosemicarbazone and/or thiosemicarbazone) in aqueous solution.

$\text{MIM}_x:\text{AldIM}_y:\text{Zn}$ (please refer to the ESI†). $\text{MIM}_{15}:\text{AldIM}_1:\text{Zn}$ was successfully prepared through hydrothermal conditions using $\text{Zn}(\text{OAc})_2$ in water/methanol at room temperature, whereas $\text{MIM}_{3.5}:\text{AldIM}_1:\text{Zn}$ was only obtained under solvothermal conditions using $\text{Zn}(\text{NO}_3)_2$ in DMF at 110 °C for 72 h. Dynamic post-synthetic modification of $\text{MIM}_{15}:\text{AldIM}_1:\text{Zn}$ and $\text{MIM}_{3.5}:\text{AldIM}_1:\text{Zn}$ was performed on the aldehyde that condenses to the amine of the bisthiosemicarbazide (Bisthio, R = $-\text{NH}_2$) or thiosemicarbazide (Thio, R = $-\text{H}$), yielding four novel TSC-ZIF: $\text{MIM}_{15}:\text{Bisthio}_1:\text{Zn}$, $\text{MIM}_{15}:\text{Thio}_1:\text{Zn}$, $\text{MIM}_{3.5}:\text{Bisthio}_1:\text{Zn}$ and $\text{MIM}_{3.5}:\text{Thio}_1:\text{Zn}$ (Scheme 1). The degree of functionalization of Ald-ZIFs was monitored by FTIR and NMR spectroscopies.

Characterisation of Ald-ZIF and TSC-ZIF

FTIR measurements. A band at 1690 cm^{-1} corresponding to the stretching $\nu(\text{C}=\text{O})$ vibration of the carbonyl group was observed in the IR spectra of $\text{MIM}_{15}:\text{AldIM}_1:\text{Zn}$ and $\text{MIM}_{3.5}:\text{AldIM}_1:\text{Zn}$. This band disappears upon introducing the TSC-functionalities, indicating successful post synthetic modification of Ald-ZIF. The conversion of the aldehyde groups, in Ald-ZIFs, to imine groups in TSC-ZIFs, was further confirmed by the strong band at 1604 cm^{-1} corresponding to the $\text{C}=\text{N}$ stretching vibration.⁷⁰ Two new IR bands are also observed at 1047 and (1864) cm^{-1} , indicative of the presence of the thiosemicarbazone group corresponding to the $\nu(\text{C}-\text{N})$ and $\nu(\text{C}=\text{S})$ stretching vibrations, respectively (Fig. S1 in the ESI†). Since the linker contains a thioamide $-\text{NH}-\text{C}=\text{S}$ functional group, it can exhibit the thione-thiol tautomerism.⁷¹ The thiol $\nu(\text{S}-\text{H})$ band around 2570 cm^{-1} is absent from the IR spectra of the TSC-ZIFs, while the $\nu(\text{N}-\text{H})$ band is present at 3153 cm^{-1} , indicating that, in the solid-state, the linker remains as the thione tautomer. The proposed IR assignments of the ZIFs are in good agreement with literature data.^{72–74} The introduction of the thioamide groups in $\text{MIM}_{3.5}:\text{Bisthio}_1:\text{Zn}$ and $\text{MIM}_{3.5}:\text{Thio}_1:\text{Zn}$ resulted in new vibrational bands, with characteristic absorptions at 2122 cm^{-1} corresponding to the $\nu_{\text{as}}(\text{NH}-\text{C}=\text{S})$ modes.⁷¹

NMR analysis. The degree of functionalization of Ald-ZIFs and TSC-ZIFs was determined by digesting the ZIFs under acidic conditions. The imine bond (linking the AldIM and the bisthio/thiosemicarbazide) does not get affected by the acidic conditions. This adopted method follows the general trend of



cleaving MOFs, where the disassembly of the MOF takes place without cleaving the imine bond.⁷⁵ Nuclear Magnetic Resonance (NMR) measurements were performed after digesting ZIF-8, Ald-ZIFs, and TSC-ZIFs in 80% deuterated solvent (DMSO-*d*₆ or D₂O-*d*₂) mixed with 20% *d*₄-acetic acid (CD₃-COOD). The chemical shifts of both imidazole linkers, 2-methylimidazole (MIM) and imidazole-4-carbaldehyde (AldIM), were referenced to DMSO-*d*₆ for MIM₁₅:AldIM₁:Zn, MIM₁₅:Bisthio₁:Zn, and MIM₁₅:Thio₁:Zn, whereas D₂O-*d*₂ was used for referencing ZIF-8, MIM_{3.5}:AldIM₁:Zn, MIM_{3.5}:Bisthio₁:Zn and MIM_{3.5}:Thio₁:Zn (see Fig. S2–S11†). The stoichiometry of the two imidazole linkers in the hybrid MIM_{*x*}:AldIM_{*y*}:Zn structures were determined by integrating the areas under the peak of the methyl protons of 2-methylimidazole and the aldehyde proton of imidazole-4-carbaldehyde (¹H NMR spectra in Fig. S4 and S7†). The carbonyl resonance of the AldIM, was also apparent at 183 ppm in ¹³C NMR of the digested MIM_{3.5}:AldIM₁:Zn (¹³C NMR spectra in Fig. S8†).

New sets of peaks were observed in the obtained NMR spectra of MIM_{*x*}:Bisthio_{*y*}:Zn and MIM_{*x*}:Thio_{*y*}:Zn; including a new peak in the aromatic range representative for the formation of the imine group HC=N, consistent with successful functionalization of the carbonyl group of AldIM with the bis/thiosemicarbazone groups. The ¹H NMR resonances of MIM_{3.5}:Thio₁:Zn correspond to the imine proton at 8.1 ppm and the three amine groups at 8.0, 7.4 and 7.9 ppm (see Fig. S10†). ¹³C NMR spectra of MIM_{3.5}:Bisthio₁:Zn and MIM_{3.5}:Thio₁:Zn exhibit two peaks at 142.03 and 178.07 ppm attributable to the C=N and C=S groups, respectively. The total transformation of the carbonyl groups in MIM_{*x*}:AldIM_{*y*}:Zn to bis/thiosemicarbazone groups was demonstrated by the absence of the aldehyde proton peak at 9.69 and 9.17 ppm, indicating a nearly complete conversion of post-synthetic modification. This was further confirmed by disappearance of the ¹³C NMR peak at 183 ppm, corresponding to the carbonyl group of the parent MIM_{3.5}:AldIM₁:Zn, in TSC-ZIFs (Fig. S9 and S11†).

Powder X-ray diffraction (PXRD) measurements. Crystallinity pattern and cubic framework structure of ZIF-8 was retained in Ald-ZIFs and TSC-ZIFs, as indicated by their PXRD diffraction data (the consistent peak positions and relative intensities as displayed in Fig. 1).¹² The PXRD diffraction patterns of the hybrid Ald-ZIF and TSC-ZIF match the diffraction patterns of the single-linker ZIF-8 structures, with all ZIFs

exhibiting virtually identical cubic unit cells. Furthermore, XRD details of the reported ZIFs indicate that all samples have relatively the same framework topology with small differences in electron density and lattice constant.

The prominent reflections at $2\theta = 7.4^\circ$, 12.7° and 18.0° for the resulting ZIFs are clear, and are in good agreement with the simulated patterns for ZIF-8 using single crystal data (Fig. S12†), with a typical SOD structure.⁶⁸

N₂ sorption-desorption isotherm. The dinitrogen sorption isotherms of the Ald-ZIFs and TSC-ZIFs were measured at 77 K, and the Brunauer–Emmett–Teller (BET) and pore volume of all the samples were calculated (Table 2 and Fig. S13†). ZIF samples were degassed overnight at 423 K before surface area determination. All ZIF samples, including the parent ZIF-8, were analysed using the same protocol since sorption behaviour for ZIFs is sensitive to handling and pre-treatment procedures.

As demonstrated in Table 2, the calculated BET surface area for ZIF-8 is $1555 \text{ m}^2 \text{ g}^{-1}$, matching reported values in the literature ($1580 \text{ m}^2 \text{ g}^{-1}$). Given that the degree of post-synthetic modification and the size of the substituents dictate the available volume for the dinitrogen adsorption within the ZIF,^{37,76} we expected the BET surface area and pore volume to decrease in the mixed-linker ZIFs, relative to ZIF-8. Indeed, all the mixed-linker ZIFs exhibit lower surface areas, with the higher aldehyde incorporation (MIM_{3.5}:AldIM₁:Zn) showing a more significant reduction in surface area than the lower aldehyde incorporation species (MIM₁₅:AldIM₁:Zn). Thus, the BET surface area of MIM₁₅:AldIM₁:Zn was found to be $1397 \text{ m}^2 \text{ g}^{-1}$, marginally lower than that of ZIF-8. Whereas, the surface area of MIM₁₅:Bisthio₁:Zn and MIM₁₅:Thio₁:Zn is reduced relative to that of MIM₁₅:AldIM₁:Zn due to the decrease of internal void space associated with the introduction of the carbonyl groups. Similarly, post-synthetic modification of MIM_{3.5}:AldIM₁:Zn results in a more significant decrease in BET surface area to 623 and $679 \text{ m}^2 \text{ g}^{-1}$ for MIM_{3.5}:Bisthio₁:Zn and MIM_{3.5}:Thio₁:Zn, respectively. This can be attributed to the higher degree of modification with bithiosemicarbazone and thiosemicarbazone groups.

SEM-EDX measurements. Surface morphology and chemical composition of Ald-ZIFs and TSC-ZIFs were also investigated using SEM (Fig. 2) and EDX (Fig. S14†). The crystals of original ZIF-8 and MIM₁₅:AldIM₁:Zn present cubic and rhombic

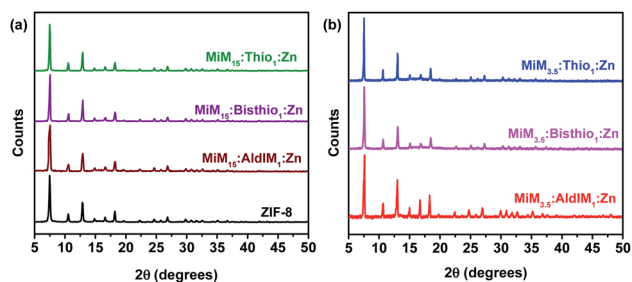


Fig. 1 PXRD pattern of the two ratios of: (a) MIM₁₅:AldIM₁:Zn, (b) MIM_{3.5}:AldIM₁:Zn.

Table 2 Textural parameters and the yields of the ZIF-8, Ald-ZIFs and the TSC-ZIFs

Sample	S_{BET}^a ($\text{m}^2 \text{ g}^{-1}$)	V_{micro}^b ($\text{cm}^3 \text{ g}^{-1}$)	Yield (%)
ZIF-8	1555	0.73	93
MIM ₁₅ :AldIM ₁ :Zn	1396	0.63	75
MIM ₁₅ :Bisthio ₁ :Zn	1128	0.5	40
MIM ₁₅ :Thio ₁ :Zn	1237	0.58	77
MIM _{3.5} :AldIM ₁ :Zn	1130	0.37	54
MIM _{3.5} :Bisthio ₁ :Zn	623	0.20	57
MIM _{3.5} :Thio ₁ :Zn	679	0.26	62

^a S_{BET} is the BET surface area. ^b V_{micro} is the *t*-plot micropore volume.



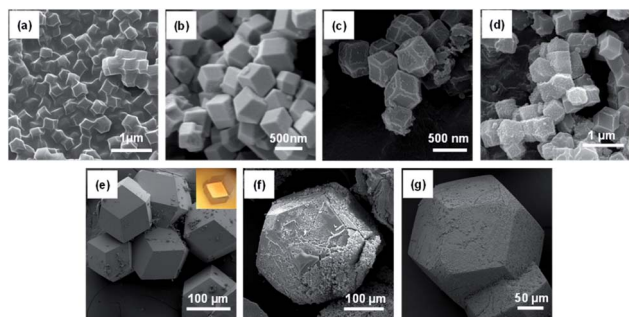


Fig. 2 SEM images for (a) ZIF-8, (b) $\text{MIM}_{15}:\text{AldIM}_1:\text{Zn}$, (c) $\text{MIM}_{15}:\text{Bisthio}_1:\text{Zn}$, (d) $\text{MIM}_{15}:\text{Thio}_1:\text{Zn}$, (e) $\text{MIM}_{3.5}:\text{AldIM}_1:\text{Zn}$ (inset: crystals of $\text{MIM}_{3.5}:\text{AldIM}_1:\text{Zn}$), (f) $\text{MIM}_{3.5}:\text{Bisthio}_1:\text{Zn}$ and (g) $\text{MIM}_{3.5}:\text{Thio}_1:\text{Zn}$.

dodecahedral shapes, respectively. Both exhibited smooth surfaces, and an average size of 500 nm. However, the surfaces of the $\text{MIM}_{15}:\text{Bisthio}_1:\text{Zn}$ sample experience a significant morphological change, as the shape changed from a rhombic dodecahedron with smooth faces and sharp edges in $\text{MIM}_{15}:\text{AldIM}_1:\text{Zn}$, to truncated-edge rhombic dodecahedra for $\text{MIM}_{15}:\text{Bisthio}_1:\text{Zn}$, but the size of the particles does not change significantly (~ 500 nm). The crystals of $\text{MIM}_{15}:\text{Thio}_1:\text{Zn}$ are rhombic dodecahedra with a bumbled surface due to the substitution of thiosemicarbazone. The crystals of $\text{MIM}_{3.5}:\text{AldIM}_1:\text{Zn}$, $\text{MIM}_{3.5}:\text{Bisthio}_1:\text{Zn}$ and $\text{MIM}_{3.5}:\text{Thio}_1:\text{Zn}$ are rhombic dodecahedral with different aspects, smooth on the surface and a large size up to $100 \mu\text{m}$ (Fig. 2).

The EDX spectra of the TSC-functionalized ZIFs confirmed that the ZIF samples are composed of C, N, O, Zn, and S, as presented in Fig. S14.† The relative content of S in the functionalized TSC-ZIFs were determined by EDX spectra.

TGAs curves analysis. Thermal stability of the prepared Ald-ZIF and TSC-ZIF samples, relative to ZIF-8, was characterised by thermal gravimetric analysis, (TGA) (Fig. S15†). Prepared Ald-ZIFs and TSC-ZIFs display relatively high thermal stability similar to that of ZIF-8. $\text{MIM}_{3.5}:\text{AldIM}_1:\text{Zn}$ undergoes an initial weight loss at about 450°C , which can be attributed to the loss of carbonyl groups of the framework. A further weight loss at 550°C is observed for ZIF-8 and $\text{MIM}_{3.5}:\text{AldIM}_1:\text{Zn}$ due to framework decomposition. $\text{MIM}_{3.5}:\text{Bisthio}_1:\text{Zn}$ and $\text{MIM}_{3.5}:\text{Thio}_1:\text{Zn}$ undergo weight loss at around 220°C , which is not present in the ZIF-8 and Ald-ZIF samples. This can be attributed to the decomposition of the bisthiosemicarbazone and thiosemicarbazone groups, respectively. However, $\text{MIM}_{15}:\text{Bisthio}_1:\text{Zn}$ and $\text{MIM}_{15}:\text{Thio}_1:\text{Zn}$ exhibit negligible percentage weight loss at this temperature due to the low percentage of the TSC-linker within the framework of the ZIF.

DFT calculations. X-ray diffraction studies show that the incorporation of imidazole-4-carbaldehyde to the framework of ZIF-8 does not alter significantly the structure of the ZIF. To get insight into the orientation of the imidazole-4-carbaldehyde (AldIM) and thiosemicarbazone group (Thio) within the structure of the ZIF, we performed DFT calculations at the b3lyp/6-31G(d,p) level.^{77–79} The X-ray crystal structure of ZIF-8 was truncated to include 24 Zn(II) ions that define the large cage of

the structure, with 8 of the 60 2-methylimidazole (MIM) (supposed to be 1 to 3.5) groups being replaced by imidazole-4-carbaldehyde. These calculations yielded the expected tetrahedral coordination of the Zn ions provided by the bridging imidazole groups, with Zn–N distances of 2.0–2.04 Å (1.97 Å in the X-ray structure).⁸⁰ Our DFT studies suggest that the carbonyl groups point inwards the six-membered hexagonal Zn rings, with the O atom being placed slightly below the mean plane defined by the six Zn ions (*ca.* 0.78 Å, Fig. 3). Indeed, changing the orientation of one of the aldehyde groups of this model towards one of the pores, defined by four ZnN_4 tetrahedra, results in a significant increase in energy of 7.8 kJ mol^{-1} . Subsequent calculations on the same model where two imidazole-4-carbaldehyde groups are replaced by thiosemicarbazone units suggest that the bulky thiosemicarbazone groups are also directed towards the large central pores of the structure.

Mercury(II) removal efficiency from water

The ability of the Ald-ZIF and TSC-ZIF derivatives to sequester mercury(II) from aqueous solutions was investigated at ambient conditions (room temperature and neutral pH). Adsorption studies were conducted over a wide range of known mercury concentrations (ppm), with the change in the adsorbent colour (yellow crystals in the case of $\text{MIM}_{3.5}:\text{Thio}_1:\text{Zn}$) to black at high mercury(II) concentrations serving as a preliminary indication of adsorption (Fig. S16†).

Equations eqn (S1) and (S2)† were used to calculate the metal removal (%) from an aqueous solution where C_i and C_e represent the initial and equilibrium metal ion concentrations (mg L^{-1}), respectively. The results for treating Hg(II) solutions with ZIF-8, Ald-ZIF and TSC-ZIF derivatives are presented in Fig. 4(a) and S17.† Treatment of a 100 mg L^{-1} aqueous Hg(II) solution with $\text{MIM}_{15}:\text{Thio}_1:\text{Zn}$ and $\text{MIM}_{15}:\text{Bisthio}_1:\text{Zn}$ led to a 92.0% and 91.8% reduction in Hg(II) content within 30 min at ambient conditions. However, treating a Hg(II) solution of the same concentration, and under the same conditions, with ZIF-8 and $\text{MIM}_{15}:\text{AldIM}_1:\text{Zn}$ resulted in 15% and 12% reduction, respectively (Fig. S17†). An obvious increase in the adsorptive removal of mercury cation was observed in TSC-ZIFs incorporating a higher degree of functionality (ratio $X_2 = 3.5$; $y_2 = 1$). Indeed,

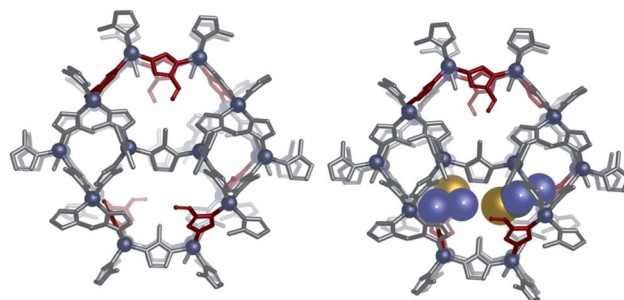


Fig. 3 Models of the ZIF-8 structure incorporating (I) imidazole-4-carbaldehyde Ald-ZIF (left) and (II) imidazole-4-carbaldehyde and thiosemicarbazone TSC-ZIF (right) groups, optimized at the b3lyp/6-31G(d,p) level.



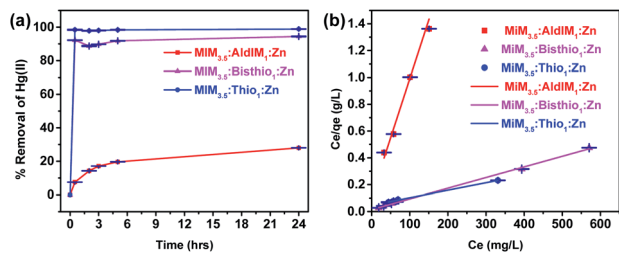


Fig. 4 (a) Percentage removal of [Hg(II)] with time using $\text{MIM}_{3.5}\text{:AldIM}_1\text{:Zn}$, $\text{MIM}_{3.5}\text{:Bisthio}_1\text{:Zn}$ and $\text{MIM}_{3.5}\text{:Thio}_1\text{:Zn}$ ($[\text{Hg(II)}] = 400 \text{ mg L}^{-1}$), (b) Langmuir equation fitting curve for the adsorption isotherms for the $\text{MIM}_{3.5}\text{:AldIM}_1\text{:Zn}$, $\text{MIM}_{3.5}\text{:Bisthio}_1\text{:Zn}$ and $\text{MIM}_{3.5}\text{:Thio}_1\text{:Zn}$.

the treatment of a Hg(II) solution ($C_i = 400 \text{ mg g}^{-1}$) with $\text{MIM}_{3.5}\text{:Thio}_1\text{:Zn}$ and $\text{MIM}_{3.5}\text{:Bisthio}_1\text{:Zn}$ resulted in 98.9% and 94.4% removal of the Hg(II) ion, respectively, with an unprecedented adsorption capacity (q_m) of 1667 mg g^{-1} and 1250 mg g^{-1} . This suggests that TSC-ZIFs possess both a high adsorption capacity and adsorption efficiency for the removal of mercury cations from water, in less than 2 hours and at ambient conditions (Fig. 4).

Adsorption isotherms for mercury(II) removal from water. The Langmuir (eqn (S3) and (S4)†), and Freundlich (eqn (S5)†) adsorption models were applied to analyse the obtained adsorption data for TSC-ZIFs. The experimental data fit well the Langmuir equilibrium adsorption isotherm with a correlation coefficient of $R^2 > 0.99$ (Fig. S18,† 4(b) and Table 3). However, the fitted Freundlich model resulted in a lower correlation coefficient ($R^2 = 0.92$, Table S1†) indicating that the adsorption process, follows a spontaneous single-layer chemical adsorption.^{67,81}

The maximum adsorption capacities of ZIFs reported in this study are presented in Table 3. The separation factor (R_L) was calculated to be between 0 and 1, indicating favourable adsorption of mercury cations into the prepared ZIFs (see Table 3). This can be attributed to the soft sulfur donor atoms incorporated in two different ratios within the pores of ZIF structures. In particular, the incorporation of bisthiosemicarbazone and thiosemicarbazone containing groups enhances mercury extraction performance with respect to the parent ZIF-8. Adsorption capacity of $\text{MIM}_{3.5}\text{:Thio}_1\text{:Zn}$ exceeds the values

Table 3 Langmuir adsorption isotherm fitting parameters for ZIF-8, Ald-ZIFs and TSC-ZIFs

Langmuir adsorption model parameters				
Samples	K_L (L mg^{-1})	R_L	q_m (mg g^{-1})	R^2
ZIF-8	0.019	0.38	3	0.9995
$\text{MIM}_{15}\text{:AldIM}_1\text{:Zn}$	0.036	0.2	13.4	0.9943
$\text{MIM}_{15}\text{:Bisthio}_1\text{:Zn}$	0.59	0.017	128	0.9961
$\text{MIM}_{15}\text{:Thio}_1\text{:Zn}$	0.15	0.062	152	0.9969
$\text{MIM}_{3.5}\text{:AldIM}_1\text{:Zn}$	0.052	0.15	124	0.9934
$\text{MIM}_{3.5}\text{:Bisthio}_1\text{:Zn}$	0.053	0.02	1250	0.9987
$\text{MIM}_{3.5}\text{:Thio}_1\text{:Zn}$	0.013	0.07	1667	0.9962

recently reported for porous functionalized ZIFs (see Table 1).^{64,65,67,68}

Adsorption kinetics. In order to evaluate the kinetic mechanism controlling the adsorption process, the effect of contact time between Hg(II) and the adsorbents on the adsorption process was investigated.

The kinetic data were successfully fitted (Fig. S19 and S20†) to the pseudo-second-order kinetic model (eqn (S6)†), as indicated by the high correlation coefficient values ($R^2 > 0.99$ for ZIF-8, $\text{MIM}_{15}\text{:AldIM}_1\text{:Zn}$, $\text{MIM}_{15}\text{:Bisthio}_1\text{:Zn}$, $\text{MIM}_{3.5}\text{:AldIM}_1\text{:Zn}$, $\text{MIM}_{3.5}\text{:Bisthio}_1\text{:Zn}$ and $R^2 = 1$ for $\text{MIM}_{15}\text{:Thio}_1\text{:Zn}$, $\text{MIM}_{15}\text{:Thio}_1\text{:Zn}$). Adsorption rate constants k_2 at room temperature and neutral pH were determined to be $0.000059 < 0.00055 < 0.0032 \text{ g mg}^{-1} \text{ min}^{-1}$ for $\text{MIM}_{3.5}\text{:AldIM}_1\text{:Zn}$, $\text{MIM}_{3.5}\text{:Bisthio}_1\text{:Zn}$ and $\text{MIM}_{3.5}\text{:Thio}_1\text{:Zn}$ respectively (Table S2†).

The adsorption rate constant ($k_2 = 0.32 \times 10^{-2} \text{ g mg}^{-1} \text{ min}^{-1}$) of $\text{MIM}_{3.5}\text{:Thio}_1\text{:Zn}$ exceeds many other reported porous adsorbents in the literature.⁶⁵ This can be attributed to the higher degree of thiosemicarbazone incorporation. The steric demands of the thiosemicarbazone group occupying the inner surface of the pores and the high density of $\text{MIM}_{3.5}\text{:Thio}_1\text{:Zn}$ adsorption sites give this TSC-ZIF the best performance.

Characterisation of TSC-ZIFs after removal of mercury(II). PXRD patterns of $\text{MIM}_{3.5}\text{:Thio}_1\text{:Zn}$ did not change after the adsorption of Hg(II) (Fig. 6(b)). The co-existence of Hg(II) with the TSC-ZIFs is observed in SEM images (Fig. S21†) and EDX analysis (Fig. S22†). Similarly, TGA measurements of the Hg(II) adsorbed onto $\text{MIM}_{3.5}\text{:Thio}_1\text{:Zn}$ show one mass loss step at about 350°C . This temperature is higher than that observed for $\text{MIM}_{3.5}\text{:Thio}_1\text{:Zn}$, confirming that the adsorbent maintained a stable framework structure after the adsorption process (Fig. S23†).

Competitive binding (binary and tertiary systems). To evaluate the selectivity of $\text{MIM}_{3.5}\text{:Thio}_1\text{:Zn}$ for Hg(II) ion adsorption, we performed experiments in the presence of Pb(II) and Cd(II) as potential interfering species.

Binary adsorption with Pb(II). Binary metal containing systems were prepared using a fixed concentration of $[\text{Pb(II)}] = 1000 \text{ mg L}^{-1}$ and a mercury concentration $[\text{Hg(II)}]$ ranging from 100 to 400 mg L^{-1} . The percentage removal of both metal ions,

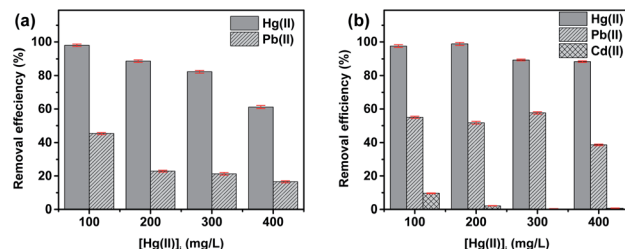


Fig. 5 (a) Mercury(II) adsorption onto $\text{MIM}_{3.5}\text{:Thio}_1\text{:Zn}$, binary system with $[\text{Pb(II)}]_i/[\text{Hg(II)}]_i$ range: 100–400 mg L^{-1} and the initial $[\text{Pb(II)}] = 1000 \text{ mg L}^{-1}$ in all samples tested, (b) mercury(II) adsorption onto $\text{MIM}_{3.5}\text{:Thio}_1\text{:Zn}$ in tertiary system with lead(II) and cadmium(II)/ $[\text{Hg(II)}]$ range: 100–400 mg L^{-1} and the initial $[\text{Pb(II)}]_i = [\text{Cd(II)}]_i = 1000 \text{ mg L}^{-1}$ in all samples tested.



existing in the binary system, is presented in Fig. 5(a). As depicted in the figure, **MIM_{3,5}:Thio₁:Zn** exhibits high removal efficiency for Hg(II) and low removal for Pb(II) ions, demonstrating a higher selectivity for Hg(II). Meanwhile, at higher mercury cations concentration, a co-adsorption induces a decrease in its adsorption. Previous studies have explained the removal of the metal ions in the competitive adsorption system is based on the comparative assessment of their initial adsorption rates.^{82,83}

Tertiary system with Pb(II) and Cd(II). The concentration of Pb(II) and Cd(II) ions in the mixed solution was set each to 1000 mg L⁻¹ and the [Hg(II)] ranging from 100 to 400 mg L⁻¹. As illustrated in Fig. 5(b), interference of the two metal ions minimally disturbs the removal efficiency for Hg(II) ions, given that **MIM_{3,5}:Thio₁:Zn** exhibits lower removal efficiency towards Cd(II) and Pb(II) ions. Analysis of the removal efficiency values revealed that the order of adsorption was Hg(II) > Pb(II) >> Cd(II). Removal efficiency for Cd(II) and Pb(II) decreases when the concentration of [Hg(II)] increases, which demonstrates the selective adsorption for Hg(II). Besides, the presence of Cd(II) in the tertiary solution enhanced the removal efficiency for Hg(II) and Pb(II) (Fig. 5(b)).

This selective adsorption for Hg(II) ions can be attributed to the higher affinity of thiosemicarbazone groups for Hg(II) compared to other metal ions.⁶⁷

Regeneration of MIM_{3,5}:Thio₁:Zn. In actual applications, reusability of adsorbents is crucial and reflects on the sustainability of the developed adsorbent. The reusability of **MIM_{3,5}:Thio₁:Zn** was assessed through cycles of regeneration of the ZIF in solution using *p*-toluene sulfonic acid (pH = 4) as a desorbent. Inspired by the literature, acidic conditions are expected to weaken the interaction between the adsorbate and adsorbent allowing for the regeneration of the **TSC-ZIF**.⁶⁸ The relative efficiency of the removal of Hg(II) in each through cycles of adsorption-desorption of mercury by **MIM_{3,5}:Thio₁:Zn** are presented in Fig. 6(a).

Over the five cycles, the amounts of mercury adsorbed decreased slightly with increasing the number of cycles, which might be caused by the loss of material during the recycling process. However, the adsorption efficiency was maintained at approximately 75% for the highest concentration of mercury(II) ([Hg(II)]_i = 700 ppm) of each cycle, indicating that **MIM_{3,5}:Thio₁:Zn** can be regenerated for cycles of mercury removal

without compromising its removal efficiency. PXRD patterns of the recycled **MIM_{3,5}:Thio₁:Zn** (after the five cycle) were in good agreement with their PXRD patterns before adsorption (Fig. 6(b)). This demonstrates the high stability of the **TSC-ZIF** after the removal of mercury.

Conclusions

A new class of aldehyde-based zeolitic imidazolate frameworks (**Ald-ZIF**) was developed to serve as a precursor, which can be modified for the removal of mercury cations from water. Bis-thiosemicarbazone and thiosemicarbazone are the functional groups introduced, through post-synthetic modification, to the new class of **Ald-ZIF** resulting in the formation of four classes of **TSC-ZIF** derivatives. **TSC-ZIF** contain pendent thiosemicarbazone groups within the pores of the material. The degree of functionalization of **Ald-ZIF** was monitored using IR and NMR spectroscopies. Structural and thermal integrity of the **TSC-ZIF** were confirmed using PXRD studies, SEM-EDX and TGA analysis. The porosity of the **TSC-ZIF** derivatives (as measured using BET surface area calculations) are reduced relative to **ZIF-8**, depending on the degree of functionalization and size of introduced substituents. Sequestration of mercury(II) from water at room temperature and neutral pH was achieved when treating Hg(II) contaminated water with **TSC-ZIF** derivatives. Among **TSC-ZIF** derivatives, **MIM_{3,5}:Thio₁:Zn** showed the highest capacity for mercury(II) ions due to the higher ratio of pore functionality, combined with the lower steric demands of the TSC group. Moreover, **MIM_{3,5}:Thio₁:Zn** showed selectivity for Hg(II) in solutions containing competitive Pb(II) and Cd(II) metal ions. **MIM_{3,5}:Thio₁:Zn** was regenerated for up to four cycles of mercury(II) removal without compromising the efficiency or structure of the ZIF. Therefore, **TSC-ZIFs**, as a new class of zeolitic frameworks, demonstrate promising adsorption capacity for heavy metals. Further work may provide a plethora of opportunities for generating new functionalized materials for other heavy metals and anions adsorption.

Conflicts of interest

There are no conflicts to declare.

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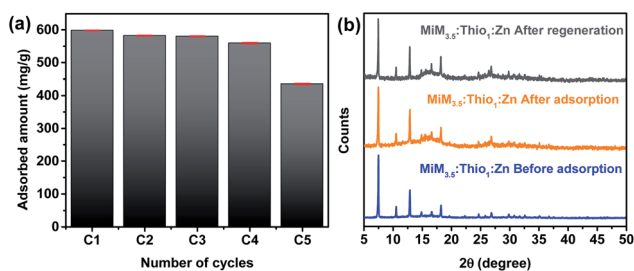


Fig. 6 (a) Reusability of **MIM_{3,5}:Thio₁:Zn** for the adsorbed amount of Hg(II) ([Hg(II)]_i = 700 ppm) and (b) PXRD patterns of the **MIM_{3,5}:Thio₁:Zn** recorded before and after the adsorption of Hg(II), and after the regeneration.

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