

Kinetic and Equilibrium Study of the reaction of nitroprusside and hydroxide ions: Influence of Ionic Strength using Pitzer Model

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Abstract

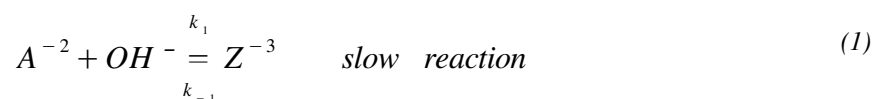
A kinetic and equilibrium study of the addition reaction of hydroxide ions to nitroprusside has been carried out in this paper. Rate and equilibrium constants at different salt concentrations (up to 4 mol/kg) were obtained and the influence of ionic strength was studied by means of Pitzer equations. This model is of special interest because it is able to explain the experimental behaviour at high ionic strength, when Debye-Huckel limiting law is no longer valid.

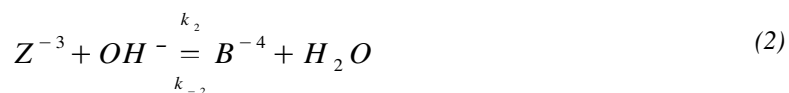
Introduction

Reactions of the nitrosyl ligand bounded to transition metal centers are interesting both in their own and in relation to the biochemical background [1] and consequently have attracted a considerable research. In particular, the reactivity of Pentacyanonitrosylferrate(II) ion has been rather extensively investigated [2,3] and numerous studies have been carried out in order to determine the electrophilic behaviour of this species [4-12]

The mechanism of the reaction between nitroprusside and hydroxide ions is well established [4-6] as well as those of the related processes with the ruthenium and osmium species [13,14]. The reaction takes place through a two-step mechanism: a rate determining attack of a hydroxide at the nitrogen, followed by the removal, by a second hydroxide, of the proton of the complex in a fast acid-base reaction.

The reactions may be written in the following form:

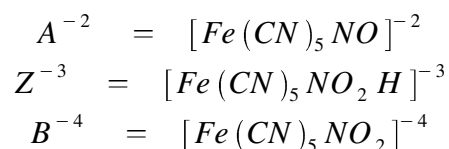




being the global process:



where stoichiometric equilibrium constant for reaction (3) will be denoted as K^* , Y^{-3} will represent the activated complex for reaction (1), and we have defined



The following rate equation has been deduced for the above process [5]:

$$v = -\frac{d[A^{-2}]}{dt} = k_{obs}[A^{-2}] \quad (4)$$

where

$$k_{obs} = k_1^* \left([OH^{-}] + \frac{1}{K^*[OH^{-}]} \right) \quad (5)$$

We made a kinetic and equilibrium study of the addition reaction of OH^{-} to $[Fe(CN)_5NO]^{2-}$: the rate constant of the first step (k_1^*) and the equilibrium constant (K^*) were determined from the value of k_{obs} . The experiments were performed at different salt concentrations and the influence of ionic strength on both constants was studied using the Pitzer equations to express the activity coefficients of the species appearing in the reactions [15,16]. The paper is organized as follows: in the experimental section determination of k_{obs} is explained, in the following section k_1^* and K^* are obtained from k_{obs} , finally in the two next sections dependence of k_1^* and K^* vs ionic strength is explained using Pitzer model.

Experimental

Chemicals of analytical reagent grade, without further purification, were used throughout this study. Solutions were prepared using doubly distilled water. Stock nitroprusside solutions were stored in the dark to prevent photochemical decomposition [17].

Reactions were carried out mixing ca. 0.5 mL of hydroxide, 0.2-1 M standardized solution, (NaOH for sodium salts, KOH for potassium salts) with ca. 3 mL of a solution containing $[\text{Fe}(\text{CN})_5\text{NO}]^{2-}$ ($2.5 \cdot 10^{-4}$ M), the inert electrolyte ($I=0.025\text{-}3$ M) and an excess of nitrite ion (0.01M) in order to prevent the aquation reaction of the product ($[\text{Fe}(\text{CN})_5\text{NO}_2]^{4-} + \text{H}_2\text{O} = [\text{Fe}(\text{CN})_5\text{H}_2\text{O}]^{3-} + \text{NO}_2^-$) [6] that could interfere with the target process (nitrite ion was added when NaCl, KCl and NaClO_4 were used)

The study of the reaction was done under pseudo first order conditions, i.e at least, a ten fold excess of $[\text{OH}^-]$. The reaction progress was followed by monitoring the appearance of $[\text{Fe}(\text{CN})_5\text{NO}_2]^{4-}$ at 400 nm with a Varian Cary 100 Bio Spectrophotometer with the cell compartment thermostated at $25 \pm 0.1^\circ\text{C}$. Rate constants, k_{obs} were determined fitting the absorbance versus time data to the first order exponential equation, using data corresponding to, at least, three half-lives.

Results and Discussion

Determination of rate and equilibrium constants

The values of k_{obs} obtained in this study are listed in table 1. The quoted rate constants have an averaged error of $\pm 0.5\text{-}2\%$. Several electrolytes were used to keep ionic strength constant.

Dependence of k_{obs} vs $[\text{OH}^-]$ is given by equation (5). The fitting of these data to equation 5 yields the rate (k_1^*) and equilibrium constants (K^*). Non-linear Marquardt algorithm has been used to perform data fitting and values obtained for k_1^* and K^* are listed in tables 2 and 3. The experimental behaviour of k_{obs} vs $[\text{OH}^-]$ is shown in figure 1. Different trends are observed depending on ionic strength: when salt concentration is low (open circles $I=0.025$ M) k_{obs} decreases with $[\text{OH}^-]$ and when it is high (solid circle $I=2\text{M}$) k_{obs} increases linearly with $[\text{OH}^-]$. This pattern has been observed for all the salts used in this study and it may be understood in view of equation (5). The second term on the right-hand side of this equation, $1/K^*[\text{OH}^-]$, includes the stoichiometric equilibrium constant, which depends strongly on the nature and concentration of the inert electrolyte [3] and increases with ionic strength; thus, for low values of K^* the second term in equation (5) predominates and results in a hyperbolic dependence of rate constant on $[\text{OH}^-]$; for the higher values of ionic strength the first term prevails and a linear dependence arises. The lacking values for the equilibrium

constant in KNO_2 ($I=3\text{M}$) and KCl ($I=2\text{M}$ and $I=3\text{M}$) is due to the impossibility of finding the K^* values that fit equation (5) because the second term it is too low to be significant.

Equilibrium and kinetic constants found in the literature are summarized in table 4, together with the corresponding ones obtained in this work. It can be seen that our data are in good agreement with the values determined by other authors.

Pitzer equations for the dependence of the equilibrium constants on the ionic strength

Equilibrium constant for reaction (3) is given by:

$$K = \frac{(B^{-4})a_w}{(A^{-2})(OH^{-})^2} = \frac{[B^{-4}]}{[A^{-2}][OH^{-}]^2} \frac{\gamma_{B^{-4}} a_w}{\gamma_{A^{-2}} \gamma_{OH^{-}}^2} = K^* \frac{\gamma_{B^{-4}} a_w}{\gamma_{A^{-2}} \gamma_{OH^{-}}^2} \quad (6)$$

where a_w denotes water activity, K^* is the stoichiometric constant and γ the activity coefficients of the species. Taking logarithms:

$$-\ln K^* = -\ln K + \ln \gamma_{B^{-4}} + \ln a_w - \ln \gamma_{A^{-2}} - 2 \ln \gamma_{OH^{-}} \quad (7)$$

Substituting in eq(7) the activity coefficients given by Pitzer model [18,19] (see Appendix 1), the result is:

$$\begin{aligned} -\ln K^* = & -\ln K + 10 f^{\gamma} + 10 I^2 B'_{MX} + 2 I (B_{MB} - B_{MA} - 2 B_{MOH}) \\ & + 2 I^2 (C_{MB} - C_{MA} - 2 C_{MOH}) + 2 I (\theta_{XB} - \theta_{XA} - 2 \theta_{XOH}) \\ & + I^2 (\psi_{MXB} - \psi_{MXA} - 2 \psi_{MXOH}) + \ln a_w \end{aligned} \quad (8)$$

where MX is the inert electrolyte. Inserting B and B' expressions, see Appendix 1, and rearranging, equation (8) becomes:

$$\begin{aligned} f_{knownI} = & -\ln K^* - 10 f^{\gamma} - 5 \beta_{MX}^{(1)} - \ln a_w = -\ln K + g (\beta_{MB}^{(1)} - \beta_{MA}^{(1)} - 2 \beta_{MOH}^{(1)}) \\ & + I (2 \beta_{MB}^{(0)} - 2 \beta_{MA}^{(0)} - 4 \beta_{MOH}^{(0)} + 2 \theta_{XB} - 2 \theta_{XA} - 4 \theta_{XOH}) \\ & + I^2 (2 C_{MB} - 2 C_{MA} - 4 C_{MOH} + \psi_{MXB} - \psi_{MXA} - 2 \psi_{MXOH}) \end{aligned} \quad (9)$$

which may be denoted as:

$$f_{knownI} = A_0 + A_1 I + A_2 g + A_3 I^2 \quad (10)$$

All known terms are included in $f_{knownI} = -\ln K^* - 10 f^{\gamma} - 5 \beta_{MX}^{(1)} - \ln a_w$. In order to use Pitzer equations, stoichiometric constants have to be converted to molality scale since they were determined in the molar scale. Conversion between concentration scales is

explained [20] in Appendix 2. Fitting of f_{known1} vs g, I, I^2 yields the values of A_1, A_2 and A_3 , as well as, thermodynamic constant, $A_0 = -\ln K$. All these parameters are listed in table 5. When KCl or KNO_2 were used as inert electrolytes, stoichiometric constants were obtained up to $I=1$ mol/dm³ and $I=2$ mol/dm³ respectively, as it has been explained in the section above. In these cases, Pitzer equations have been used without quadratic terms, which are negligible at low ionic strength (less than $I=2$). In figure 2, experimental data are shown together with fitting functions, according to Pitzer model. At low ionic strength, where Debye-Huckel limiting law is still valid, the behaviour is quite similar for all the electrolytes, however when salt concentration is increased different trends are observed. Equilibrium constants in potassium salts exhibit higher values than those in sodium salts (making their determination impossible at ionic strengths higher than 1), and it is also observed that this behaviour depends on the cation (curves for sodium salts and for potassium salts, make two clearly different groups). This is the expected behaviour because the species involved in the equilibrium bear negative charge, so they interact with cations in a greater extent than with anions.

Pitzer equations for the dependence of the rate constant on the ionic strength

The rate constant for an elemental reaction at a certain ionic strength, k_1^* , is related to the rate constant at zero ionic strength, k_1^0 , by means of the following equation [21]:

$$k_1^* = k_1^0 \frac{\gamma_{A^{-2}} \gamma_{OH^-}}{\gamma_{Y^{-3}}} \quad (11)$$

where Y^{-3} represents the activated complex. Taking logarithms:

$$\ln k_1^* = \ln k_1^0 + \ln \gamma_{A^{-2}} + \ln \gamma_{OH^-} - \ln \gamma_{Y^{-3}} \quad (12)$$

substituting the activity coefficients according to Pitzer equations (see Appendix 1)

$$\begin{aligned} f_{\text{known2}} = \ln k_1^* + 4 f^Y + 2 \beta_{MX}^{(1)} g' &= \ln k_1^0 + g \left(\beta_{MA}^{(1)} + \beta_{MOH}^{(1)} - \beta_{MY}^{(1)} \right) \\ &+ I \left(2 \beta_{MA}^{(0)} + 2 \beta_{MOH}^{(0)} - 2 \beta_{MY}^{(0)} + 2 \theta_{XA} + 2 \theta_{XOH} - 2 \theta_{XY} \right) \\ &+ I^2 \left(2 C_{MA} + 2 C_{MOH} - 2 C_{MY} + \psi_{MXA} + \psi_{MXOH} - \psi_{MXY} \right) \end{aligned} \quad (13)$$

which may be denoted as:

$$f_{\text{known2}} = B_0 + B_1 I + B_2 g + B_3 I^2 \quad (14)$$

All known terms are included in $f_{known2} = \ln k_1^* + 4 f^y + 2 \beta_{MX}^{(1)} g'$. In order to use Pitzer equations, the rate constants have been converted to molality scale as it is described in Appendix 2. Fitting of f_{known2} vs g, I, I^2 yields the values of B_1, B_2 and B_3 , as well as, the rate constants at zero ionic strength, $B_0=k^0$. All these parameters are listed in table 6. In figure 3, experimental data are shown together with fitting functions, according to Pitzer model. As it was to be expected when the reacting species have the same sign, an increase in ionic strength increases the rate, with a similar behaviour for all the electrolytes. This is true at low salt concentration when limiting law is still valid [21]. However, at higher ionic strengths, when this law is not good enough to describe the dependence of activity coefficients on ionic strength, rate constants do not increase as rapid as they did (or they even decrease). Besides, their values differ from one electrolyte to another. This effect is more important the greater is the salt concentration, in this situation the use of interaction models for the activity coefficient, ie Pitzer model, is clearly needed to explain the experimental behaviour.

Errors in Pitzer parameters

Since its outset, the Pitzer approach has found wide and successful application in reproducing experimental data for complex systems. However, difficulties arise because, in some cases, the resulting intercorrelation among the variables in the regression, due to multicollinearity, may lead to highly imprecise parameter estimates, as can be seen in our case, in table 5 (parameter A_1 for NaClO_4 and NaCl) and in table 6 (parameters B_1 and B_3). Our group and others have applied in some cases alternative procedures in order to overcome the multicollinearity problem, as, for example, ridge regression method [22-25]. However, this alternative method leads theoretically to more precise, but slightly biased estimates for the parameters in the model. In order to avoid the controversy over the performance of the ridge regression method [26], a common practice [27,28] is to simply omit some parameters in the model as it would be the case for A_1 in table 5 or B_3 in table 6.

Appendix 1: Pitzer equations for activity coefficients

In this appendix activity coefficients of the species involved in reactions (1) and (2) are expressed by means of Pitzer model. Inert electrolyte, represented by MX, is in great excess in relation to other species. If $z_{M^+} = 1$ and $z_{X^-} = -1$, the ionic strength is given by $I = m_{M^+} = m_{X^-}$. The activity coefficient of an ion i , bearing negative charge, z_i , according to Pitzer theory is giving by [18]:

$$\ln \gamma_i = z_i^2 f^y + 2 I (B_{Mi} + I C_{Mi}) + 2 I \theta_{iX} + I^2 (z_i^2 B'_{MX} + z_i C_{MX} + \psi_{iMX})$$

where, f^y is a extended form of the Debye-Hückel term that takes into account long-range interactions, and it is given, at 25°C, by [18]:

$$f^y = -0.3915 \left[\frac{\sqrt{I}}{1 + 1.2 \sqrt{I}} + \frac{2}{1.2} \ln(1 + 1.2 \sqrt{I}) \right]$$

B, the second virial coefficient, and its derivative, B', are defined in Pitzer theory by:

$$B_{MX} = \beta_{MX}^{(0)} + \frac{\beta_{MX}^{(1)}}{2I} \left[1 - (1 + 2\sqrt{I}) e^{-2\sqrt{I}} \right] = \beta_{MX}^{(0)} + \frac{\beta_{MX}^{(1)}}{2I} g$$

$$B'_{MX} = \frac{\beta_{MX}^{(1)}}{2I^2} \left[-1 + (1 + 2I + 2\sqrt{I}) e^{-2\sqrt{I}} \right] = \frac{\beta_{MX}^{(1)}}{2I^2} g'$$

where we have called $g = 1 - (1 + 2\sqrt{I}) e^{-2\sqrt{I}}$ and $g' = -1 + (1 + 2I + 2\sqrt{I}) e^{-2\sqrt{I}}$

The interaction parameters $\beta_{MX}^{(0)}$, $\beta_{MX}^{(1)}$ are specific to the compound MX, and they represent the short-range interaction in the presence of the solvent between solute particles M and X. The third virial coefficient, C_{MX} , represents triple interactions MMX and XXM.

Parameter θ_{iX} accounts for interactions between ions of like sign (i and X), which arises only for mixed solutions. The same is true for the term ψ_{iMX} , that it is related to the triple interactions of two similarly charged ions (i and X) with and ion of opposite charge (M).

Therefore, the activity coefficient for the ions involved in reactions (1) and (2) are:

$$\ln \gamma_{OH^{-1}} = f^y + 2 I (B_{MOH} + I C_{MOH}) + 2 I \theta_{XOH} + I^2 (B'_{MX} + C_{MX} + \psi_{OHMX})$$

$$\ln \gamma_{A^{-2}} = 4 f^y + 2 I (B_{MA} + I C_{MA}) + 2 I \theta_{AX} + I^2 (4 B'_{MX} + 2 C_{MX} + \psi_{AMX})$$

$$\ln \gamma_{Y^{-3}} = 9 f^y + 2 I (B_{MY} + I C_{MY}) + 2 I \theta_{YX} + I^2 (9 B'_{MX} + 3 C_{MX} + \psi_{YMX})$$

$$\ln \gamma_{B^{-4}} = 16 f^y + 2 I (B_{MB} + I C_{MB}) + 2 I \theta_{BX} + I^2 (16 B'_{MX} + 4 C_{MX} + \psi_{BMX})$$

On the other hand, in equation (6) it appears the activity of water, a_w , that is related to the osmotic coefficient, ϕ , by the following equation [19]:

$$\ln a_w = \frac{-M_0 I}{1000} \phi$$

where $M_0=18$ is the molar mass of the solvent and the osmotic coefficient can be expressed by means of Pitzer theory as follows [18]:

$$\phi - 1 = -0.3915 \left[\frac{\sqrt{I}}{1 + 1.2 \sqrt{I}} \right] + I \left(\beta_{MX}^{(0)} + \beta_{MX}^{(1)} e^{-2\sqrt{I}} \right) + I^2 C_{MX}^\phi$$

where C is related to C^ϕ by:

$$C_{MX} = \frac{C_{MX}^\phi}{2 |z_{M^+} z_{X^-}|^{1/2}},$$

in salts of 1-1 valence type $z_{M^+} = 1$, $z_{X^-} = -1$ and $C_{MX} = \frac{C_{MX}^\phi}{2}$

Table 7 gives the Pitzer parameters used to calculate the osmotic coefficient and the water activity for the inert salts used in this study.

Appendix 2: Interconversion of concentration scales

Equilibrium and rate constants have been determined using molar concentration scale, but in order to apply Pitzer equations, it is necessary to use the molality scale. The relationship between molality, m_i , and molarity, c_i , for species i in a solution with a density ρ , is expressed by the following equation:

$$m_i = \frac{c_i}{\rho - M_{salt} c_{salt}}$$

where M_{salt} is the molar mass of the salt. As it can be seen, to perform the conversion between concentration scales, density of solutions is needed. The concentration of the inert electrolyte is much higher than that of the reacting species, so density of solutions has been considered equal to that of solutions containing only the salt, that was taken from ref [20]

Taking into account last equation, stoichiometric equilibrium constant is given by:

$$K^* = \frac{m_{B^{-4}}}{m_{A^{-2}} m_{OH^-}^2} = \frac{c_{B^{-4}}}{c_{A^{-2}} c_{OH^-}^2} (\rho - M_{salt} c_{salt})^2 = K_c^* (\rho - M_{salt} c_{salt})^2$$

where K^* is the constant in the molal scale and K_c^* is the corresponding one in the molar scale.

Taking logarithms: $\log K^* = \log K_c^* + 2 \log (\rho - M_{salt} c_{salt})$

The conversion equation for rate constant may be obtained by similar reasoning:

$$\log k_1^* = \log k_{1c}^* + \log (\rho - M_{salt} c_{salt})$$

where k^* is the constant in the molal scale and k_c^* is in the molar scale.

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Table 1. Rate constant data, k_{obs} , see eq (5), for the reaction of nitroprusside with OH^- in aqueous solution at 25°C.

NaNO ₂					
$I/\text{mol L}^{-1}$	$10^3 \times [\text{OH}^-]/\text{mol L}^{-1}$	$10^3 \times k_{\text{obs}}/\text{s}^{-1}$	$I/\text{mol L}^{-1}$	$10^3 \times [\text{OH}^-]/\text{mol L}^{-1}$	$10^3 \times k_{\text{obs}}/\text{s}^{-1}$
0.03	5.05	8.90	0.5	7.21	3.06
	7.01	6.60		14.4	4.94
	8.98	5.69		21.6	7.18
	10.9	5.10		28.8	9.43
	12.9	4.84		36.1	11.6
	14.9	4.64		43.3	14.0
0.05				50.5	16.1
	5.41	6.34		54.1	17.0
	10.8	4.46	1	7.21	3.18
	19.8	4.67		14.4	5.55
	25.2	5.26		21.6	8.16
	30.6	6.61		28.8	10.8
	36.1	6.42		36.1	13.0
	39.7	7.04		43.3	15.7
43.3	7.52				
0.1	3.16	6.48	2	7.21	3.71
	6.31	4.22		14.4	6.89
	12.6	3.82		21.6	10.3
	18.9	4.58		28.8	13.9
	25.2	5.62		36.1	16.7
	31.6	6.83		43.3	20.6
	44.2	9.33		50.5	24.3
		61.7	28.8		
0.2	7.21	3.38	3	5.05	2.93
	18.0	4.87		7.01	3.99
	28.8	7.52		8.98	5.04
	39.7	10.0		10.9	6.09
	50.5	12.1		12.9	7.41
	61.3	15.2		14.9	8.63
	72.1	17.3			
	90.1	21.7			

KNO₂

I/ mol L ⁻¹	10 ³ x[OH ⁻]/ mol L ⁻¹	10 ³ xk _{obs} /s ⁻¹	I/ mol L ⁻¹	10 ³ x[OH ⁻]/ mol L ⁻¹	10 ³ xk _{obs} /s ⁻¹	
0.03	6.33	6.01	0.2	39.9	11.7	
	7.02	5.72		50.3	14.7	
	8.06	5.33				
		9.02	5.12			
		10.1	4.76	0.5	6.33	2.81
		11.0	4.65		10.1	4.06
		12.5	4.50		15.0	5.88
			19.9		7.78	
0.05	6.33	4.54		25.1	9.75	
	9.02	4.07		29.9	11.9	
	12.1	4.01		39.9	15.6	
	15.0	4.18		50.3	19.6	
	18.2	4.53				
	19.9	4.76	1	6.33	3.30	
	25.1	5.59		10.1	5.06	
		15.6		7.75		
0.1	6.33	2.81		19.9	9.86	
	10.1	4.06		29.9	14.7	
	15.0	5.88				
	19.9	7.78	2	6.33	4.07	
	25.1	9.75		10.1	6.63	
	29.9	11.9		15.0	8.97	
	39.9	15.6		19.9	12.1	
	50.3	19.6		25.1	15.5	
0.2	6.33	3.00	3	4.89	3.31	
	10.1	3.59		6.93	5.07	
	15.0	4.81		8.98	6.29	
	19.9	6.12		11.0	7.97	
	25.1	7.46		13.1	9.59	
	29.9	8.75		14.9	10.8	

NaCl

$I/\text{mol L}^{-1}$	$10^3 \times [\text{OH}^-]/\text{mol L}^{-1}$	$10^3 \times k_{\text{obs}}/\text{s}^{-1}$	$I/\text{mol L}^{-1}$	$10^3 \times [\text{OH}^-]/\text{mol L}^{-1}$	$10^3 \times k_{\text{obs}}/\text{s}^{-1}$
0.03	5.05	8.18	0.5	5.05	2.74
	7.01	6.38		7.01	2.84
	8.98	5.36		8.98	3.28
	10.9	4.89		10.9	3.83
	12.9	4.70		12.9	4.24
				14.9	4.78
0.05	5.05	6.29	1	5.05	2.44
	7.01	5.23		7.01	3.00
	8.98	4.62		8.98	3.76
	10.9	4.38		10.9	4.50
	12.9	4.29		12.9	5.09
	14.9	4.28		14.9	5.89
0.1	5.05	4.85	2	5.05	2.90
	7.01	4.24		7.01	3.96
	8.98	3.91		8.98	4.84
	10.9	3.82		10.9	5.96
	12.9	3.96		12.9	6.89
	14.9	4.12		14.9	8.09
0.2	5.05	3.59	3	5.05	3.10
	7.01	3.39		7.01	4.24
	8.98	3.48		8.98	5.38
	10.9	3.66		10.9	6.71
	12.9	3.89		12.9	7.87
	14.9	4.26		14.9	9.38

KCl

$I/\text{mol L}^{-1}$	$10^3 \times [\text{OH}^-]/\text{mol L}^{-1}$	$10^3 \times k_{\text{obs}}/\text{s}^{-1}$	$I/\text{mol L}^{-1}$	$10^3 \times [\text{OH}^-]/\text{mol L}^{-1}$	$10^3 \times k_{\text{obs}}/\text{s}^{-1}$
0.03	4.89	6.32	0.5	4.89	2.15
	6.93	4.79		6.93	2.69
	8.98	4.25		8.98	3.30
	11.0	3.96		11.0	4.06
	13.1	3.84		13.1	4.75
				14.9	5.31
0.05	4.89	4.52	1	4.89	2.45
	6.93	3.82		6.93	3.25
	8.98	3.49		8.98	4.16
	11.0	3.46		11.0	5.21
	13.1	3.50		13.1	6.13
	14.9	3.64		14.9	6.89
0.1	4.89	3.30	2	4.89	3.06
	6.93	3.04		6.93	4.47
	8.98	3.08		8.98	5.78
	11.0	3.27		11.0	7.07
	13.1	3.46		13.1	8.43
	14.9	3.81		14.9	9.84
0.2	4.89	2.54	3	4.89	3.52
	6.93	2.63		6.93	5.23
	8.98	3.00		8.98	6.66
	11.0	3.45		11.0	8.32
	13.1	3.88		13.1	9.63
	14.9	4.29		14.9	11.3

NaClO₄

I/ mol L ⁻¹	10 ³ x[OH ⁻]/ mol L ⁻¹	10 ³ xk _{obs} /s ⁻¹	I/ mol L ⁻¹	10 ³ x[OH ⁻]/ mol L ⁻¹	10 ³ xk _{obs} /s ⁻¹
0.03	5.05	8.72	0.5	5.05	2.77
	7.01	6.74		7.01	2.91
	8.98	5.62		8.98	3.31
	10.9	5.01		10.9	3.72
	12.9	4.82		12.9	4.22
				14.9	4.74
0.05	5.05	6.45	1	5.05	2.42
	7.01	5.14		7.01	2.90
	8.98	4.48		8.98	3.46
	10.9	4.25		10.9	4.11
	12.9	4.16		12.9	4.67
	14.9	4.22		14.9	5.39
0.1	5.05	4.78	2	5.05	2.05
	7.01	4.05		7.01	2.74
	8.98	3.80		8.98	3.42
	10.9	3.81		10.9	4.14
	12.9	3.86		12.9	4.88
	14.9	4.09		14.9	5.91
0.2	5.05	3.70	3	5.05	1.86
	7.01	3.40		7.01	2.55
	8.98	3.42		8.98	3.21
	10.9	3.60		10.9	3.87
	12.9	3.82		12.9	4.70
	14.9	4.19		14.9	5.56

Table 2. Stoichiometric equilibrium constants, K^* , for reaction (3) obtained from fitting of data in table 1 to eq (5), $T=25^\circ\text{C}$.

	NaNO ₂	NaCl	NaClO ₄	KNO ₂	KCl
$I/\text{mol L}^{-1}$	$10^{-3} K^*$	$10^{-3} K^*$	$10^{-3} K^*$	$10^{-3} K^*$	$10^{-3} K^*$
0.025	3.1±0.1	3.6±0.1	3.0±0.1	4.9±0.2	4.8±0.2
0.05	5.65±0.07	6.0±0.2	5.3±0.1	8.8±0.1	8.8±0.1
0.1	10.7±0.2	9.4±0.2	9.6±0.1	17.9±0.3	17.9±0.3
0.2	20±2	18.5±0.3	16.9±0.2	40±2	43±1
0.5	53±9	47±2	44±1	218±68	170±16
1	78±19	141±15	102±6	411±311	629±240
2	216±186	385±107	430±39	301±252	
3	510±59	727±63	686±162		

Table 3. Second order rate constants, k_1^* , obtained from fitting of data in table 1 to eq (5), $T=25^\circ\text{C}$.

	NaNO ₂	NaCl	NaClO ₄	KNO ₂	KCl
$I/\text{mol L}^{-1}$	$k_1^*/\text{M}^{-1}\text{s}^{-1}$	$k_1^*/\text{M}^{-1}\text{s}^{-1}$	$k_1^*/\text{M}^{-1}\text{s}^{-1}$	$k_1^*/\text{M}^{-1}\text{s}^{-1}$	$k_1^*/\text{M}^{-1}\text{s}^{-1}$
0.025	0.127±0.005	0.137±0.004	0.123±0.005	0.157±0.007	0.132±0.005
0.05	0.158±0.001	0.166±0.005	0.152±0.003	0.186±0.001	0.162±0.002
0.1	0.198±0.002	0.187±0.004	0.185±0.002	0.232±0.001	0.203±0.002
0.2	0.240±0.001	0.229±0.002	0.220±0.002	0.288±0.001	0.261±0.002
0.5	0.316±0.002	0.291±0.004	0.288±0.002	0.389±0.001	0.349±0.002
1	0.362±0.003	0.380±0.003	0.345±0.002	0.491±0.004	0.461±0.003
2	0.472±0.003	0.529±0.004	0.372±0.001	0.607±0.009	0.648±0.004
3	0.546±0.002	0.588±0.002	0.351±0.002	0.720±0.008	0.749±0.005

Table 4.a) Stoichiometric equilibrium constants, K^* , for reaction (3)

Reference	Method	K^*	I/(mol L ⁻¹)
12	Polarography spectrophotometry this work	1.1×10^6 1×10^6 $(1.7 \pm 0.2) \times 10^5$	0.5(KCl)
6	Spectrophotometric this work	$(1.5 \pm 0.3) \times 10^6$ $(1.41 \pm 0.15) \times 10^5$	1(NaCl), 0.03(NO ₂ ⁻)
4	polarography and spectrophotometry this work	3.17×10^4 $(5.3 \pm 0.9) \times 10^4$	0.5 (NaNO ₂)
5	Stopped flow this work this work	1.26×10^4 $(1.69 \pm 0.02) \times 10^4$ $(4.4 \pm 0.1) \times 10^4$	0.35(NaClO ₄), 0.1(NaNO ₂), 23°C 0.2(NaClO ₄) 0.5(NaClO ₄)
11	Stopped flow	1.86×10^4	0.5 (LiClO ₄)

b) Rate constants for the bimolecular reaction, k_1^* , see eq. (1)

Reference	Method	$k_1^*/M^{-1}s^{-1}$	I/(mol L ⁻¹)
6	Spectrophotometry this work	0.55 ± 0.01 0.380 ± 0.003	1(NaCl) excess NO ₂ ⁻
4	polarography this work	0.216 0.316 ± 0.002	0.5 (NaNO ₂)
5	Stopped flow this work this work	0.202 ± 0.002 0.220 ± 0.002 0.288 ± 0.002	0.35(NaClO ₄), 0.1(NaNO ₂), 23°C 0.2(NaClO ₄) 0.5(NaClO ₄)

Table 5. Interaction parameters of equation (10) at 25°C

	A_0	A_1	A_2	A_3
KCl	-6.88 ± 0.03	0.5 ± 0.2	0.8 ± 0.3	
KNO₂	-6.71 ± 0.09	2.3 ± 0.2	-2.5 ± 0.5	
NaClO₄	-6.63 ± 0.08	-0.5 ± 0.5	4.9 ± 0.8	0.16 ± 0.09
NaCl	-6.69 ± 0.06	-0.3 ± 0.3	4.3 ± 0.6	0.12 ± 0.07
NaNO₂	-6.57 ± 0.10	1.6 ± 0.6	2 ± 1	-0.3 ± 0.1

Table 6. Interaction parameters of equation (14) at 25°C

	B_0	B_1	B_2	B_3
KCl	-2.60 ± 0.02	-0.2 ± 0.1	-1.6 ± 0.2	-0.009 ± 0.03
KNO₂	-2.459 ± 0.006	-0.27 ± 0.04	-1.41 ± 0.06	0.018 ± 0.007
NaClO₄	-2.66 ± 0.01	-0.42 ± 0.09	-1.7 ± 0.1	0.004 ± 0.02
NaCl	-2.54 ± 0.02	0.3 ± 0.1	-2.7 ± 0.2	-0.09 ± 0.02
NaNO₂	-2.62 ± 0.03	-0.4 ± 0.2	-1.5 ± 0.3	0.04 ± 0.03

Table 7. Pitzer parameters from ref [18] at 25°C

	$\beta^{(0)}$	$\beta^{(1)}$	C^ϕ
KCl	0.04835	0.2122	-0.00084
KNO₂	0.0151	0.015	0.0007
NaClO₄	0.0554	0.2755	-0.00118
NaCl	0.0765	0.2664	0.00127
NaNO₂	0.0641	0.1015	-0.0049

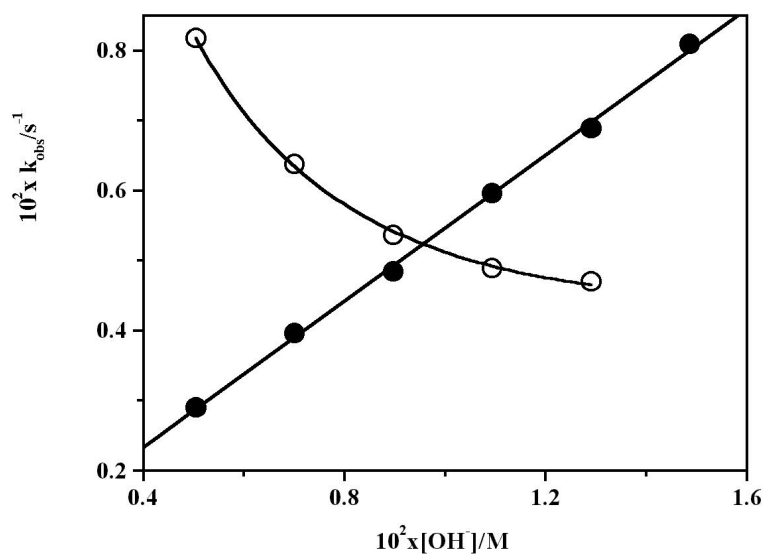


Fig. 1. Plot of k_{obs} vs. $[OH^-]$ for $[Fe(CN)_5NO]^{2-} = 2.5 \times 10^{-4} M$, $[NaNO_2] = 0.01 M$, 25°C. Open circles $I = 0.025 M$ (NaCl), solid circles $I = 2 M$ (NaCl). The lines correspond to the theoretical behaviour derived from equation 5.

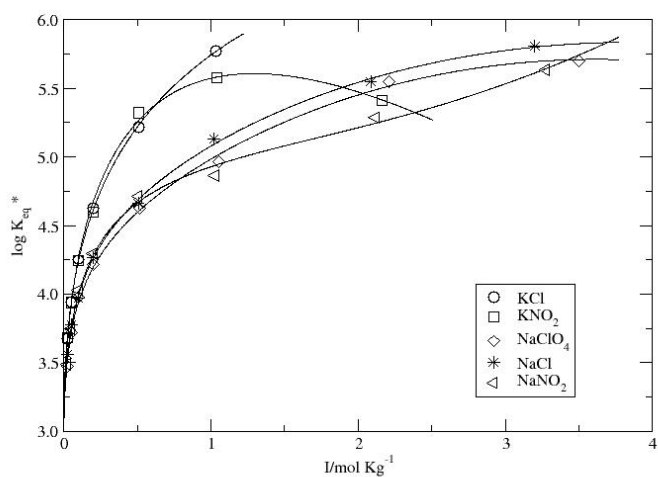


Fig.2 Stoichiometric equilibrium constant vs ionic strength: experimental data and Pitzer model

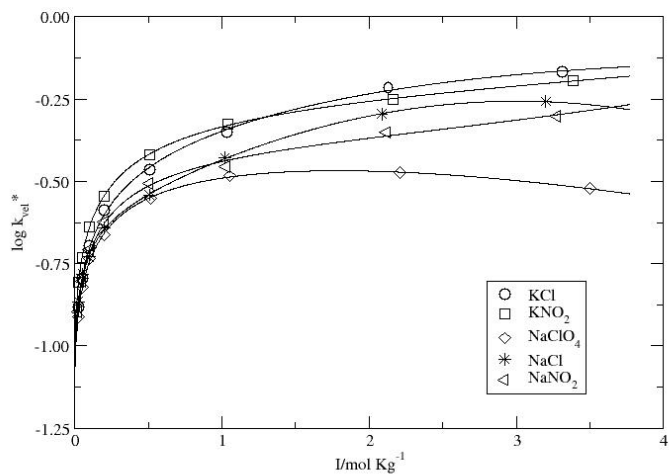


Fig.3 Rate constant vs ionic strength: experimental data and Pitzer model